## Heritage Science

### **RESEARCH ARTICLE**

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# Microclimate numerical simulation to obtain the minimum safe distances between a painted wood panel and the inner face of an exterior wall

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#### **Abstract**

This study provides a detailed understanding of the heat fluxes and temperatures that take place in the *channel* between the inner face of an exterior wall and the back of a painted wood panel hung on it. This is performed by means of a numerical simulation with a 2 dimensional CFD software. Distributions of temperatures, heat fluxes, and other parameters are quantified for 56 cases where the classical equations—Raithby-Hollands and similar—cannot be applied as these require vertical isothermal plates or isofluxes. Studied scenarios include different panel heights, *channel* widths, and room heights. Combining these data with outside temperature (– 3 °C) and heating air supply temperature (20 °C), to provide a nearly constant 19.6 °C in the room except in the channel between panel and wall, and with two values of specific humidity in the room, we provide for every studied case, advised distances, for these conditions, between the panel and the wall.

**Keywords:** Museum microclimates, CFD model, Numerical simulation, Wall condensation, Easel painting condensation, Thermal convection

#### Introduction

If we place an easel painting or a painted wood panel in the interior face of an exterior wall (either touching the wall or very close to it) both act as thermal insulators. So, in historical buildings with non-thermally insulated exterior walls and low outside temperatures, the inside wall face and the painting back temperatures can drop some degrees below the room temperature and consequently the relative humidity (RH) in these places can rise to unacceptable levels for the proper conservation of paintings [1]. Neuhaus [2] states that in this case, spacers shall be placed between paintings and wall in order to provide insulation at the painting back but required distances are not provided.

In Padfield previous study [3] temperature and RH have been measured on site and a minimum distance of 20 mm has been recommended between a 35 cm high framed painting and the inner face of a window facing north. Although broader distances have been suggested for bigger artefacts, specific values have not been calculated for this or other scenarios.

The aim of this research is not to set the exhibition room climatic conditions in historical buildings, which today in Europe are established by the CEN recommendations but to calculate the temperatures and heat flux distributions in the *channel* between a cold exterior wall and painted wood panels of different sizes placed at varying distances from the wall and at two different relative humidity values, to extend the general recommendation given in the Padfield study. Performing measurements on site requires large number of tests in different and very accurate environment conditions. The differential

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equations that model heat transfer in fluids take into account three fundamental laws as the mass, momentum and energy conservation, and thus theoretically, they can solve the heat transfer simulation between the fluid and the boundaries in whatever complex geometry. However, as they are in not linear partial derivatives, they can be solved analytically only in a few particular cases through dimensional analysis and simplifications.

Heat transfer between two parallel vertical isothermal and isoflux plates through the air by natural convection has been well parametrized by Raithby-Hollands [4], Bar-Cohen [5], Cadafalch-Oliva [6], Spalding [7, 8], and others, but as the exterior wall and the wood panel are neither isothermal and nor isoflux plates, their equations cannot be applied.

Instead, at present, CFD tools offer the possibility to solve numerically differential equations that model heat transfer in our selected geometry and materials with enough accuracy and at a reasonable cost. The commercial 2D fluid mechanics software EasyCFD\_G developed and tested by A. Gameiro of the Coimbra University [9–14], is used in this research to extend the only existing single recommendation, up to now, of minimum 20 mm for the distance between a "cold" external wall in historical buildings and a painting hung on it.

This tool allows us to use the  $(k-\omega)$  or the  $(k-\varepsilon)$  equations, where k is for turbulent kinetic energy,  $\varepsilon$  for its dissipation rate,  $\omega$  for the turbulent kinetic energy frequency of dissipation, according to the distance from each mesh element to the boundaries and to quantify some magnitudes, raised in the Grau-Bové and Strlic article [15] such as the turbulence and the thermal fluxes in each mesh element, distinguishing between the contributions by convection and conduction.

These simulations show important vertical temperature gradients at the wall and the wood panel back when the room heating air supply (20 °C) provides a nearly constant value (19.6 °C  $\pm$  0.3 K) around the room (except in corners and in the space between the back of the panel and the wall).

The specific humidity (SH) is considered constant in all the room. The possible water buffer action from the boundary surfaces (walls and panel) is not considered, as the simulations are done for a steady state and this allows to simplify the problem and to get an easier understanding of the heat fluxes involved. Two SH scenarios are considered (7.5 g/kg and 8.7 g/kg) which correspond to 52% RH and 60% RH both at 19.6 °C.

From this point on, *Wall* refers to the inner face of the exterior wall, *Back* to the wood panel surface facing the *channel* and *Front* to the wood panel surface facing the room. Also the space between the inner side of the exterior wall and the back of the panel is named *channel*.

#### Materials and methods

#### Simulation description

We have built 8 different 2-dimensional CFD "models", each of them composed by a vertical cross-section of a room 3 m wide with a 2 cm thick wood panel hanging at different distances ("s") from the *Wall*. From this point on, the word *panel* will be used with the same meaning as wood panel.

All the models also have the same following features: heating system by hot air forced convection, distance from the panel centre to the floor (1.5 m) and boundary conditions. The difference among the 8 models lies in the following variables: different panel height "h" (2 m, 1 m and 0.5 m), different room height "ht" (3 m and 6 m) to quantify the effect of the distance travelled by the air along the cooled inner face of the Wall before entering in the channel, one model without the panel (for comparison) and another model in a room 6 m high with a cornice 15 cm high and 5 cm wide protruding from the inner side of the outside wall at 30 cm above the wood panel.

For each of the 8 described models, there are different "cases" (one for each distance "s" from panel to wall), see Table 1. Combining all the mentioned variables, we get 45 basic cases. All basic cases and models are listed in Table 1. See sketch in Fig. 1.

Doing it we have simulated 45 basic cases where in a heated room of different heights, painted wood panels of different dimensions (models) are hung at different short distances on the inner face of an exterior wall.

In these simulations we got air velocities (u horizontal and v vertical), temperatures (Tw wall, Tb back and Ta air), heat fluxes and turbulence intensity (Tu) for each of

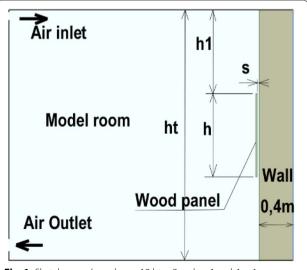


Fig. 1 Sketch room/panel case 12 ht=3 m, h=1 m, h1=1 m, s=20 mm

Table 1 Su	Table 1 Summary of the 45 basic cases data	45 basic	: cases data										
Panel height	Channel width	1	Distance from panel to the ceiling	Room wall height	Mesh cells	Cell rows in <i>Channel</i> Width	Total iterations	Total iterations Initial time step subrelax factor	Next time step subrelax factor	Next time step subrelax factor	Class	Model	Case
٩	s	s/h	h1	þţ	1	ı	ı	ı	1	1	ı		1
E	mm	Ratio	E	٤	n°	n°	n°	I	ı	ı	ı	·	ı
2	40	0.020	0.5	т	70,847	16	2968	0.1	0.02	ı	-	_	
	30	0.015			65,714	12	2471	0.1	0.02	ı	-		2
	25	0.0125			68,442	10	3023	0.1	0.02	1	-		$\sim$
	20	0.010			64,526	∞	4971	0.1	0.02	ı	-		4
	15	0.0075			11,8332	11/12	3495	0.1	0.02	ı	<b>-</b>		2
	10	0.0050			11,0785	80	1775	0.1	1	I	-		9
	5	0.0025			17,8393	9	6971	0.1	1	I	-		7
	3	0.0015			12,1399	6/9	2925	0.1	0.02	I	<del></del>		∞
	2.5	0.0013			13,1171	5/7	1257	0.1	ı	ı	<b>-</b>		6
	2	0.0010			11,6523	4/6	1213	0.1	ı	1	-		01
	0	0.000			56,490	0	2644	0.1	0.02	ı	-		11
-	20	0.020	_	3	47,763	8	2342	0.1	0.02	I	<del></del>	2	12
	15	0.015			46,880	7	3686	0.1	0.02	ı	<b>-</b>		13
	12.5	0.0125			76,151	11	2119	0.1	ı	ı	<del></del>		4
	10	0.010			76,889	6	3012	0.1	0.02	I	<del></del>		15
	7.50	0.0075			102253	12	4599	0.1	0.02	ı	<b>-</b>		16
	5	0.0050			26,777	80	3748	0.1	0.02	I	-		17
	2.5	0.0025			91,920	4	2380	0.1	1	I	-		18
	1.5	0.0015			15,4030	4/5	1535	0.1	0.02	I	_		19
	0	0.000			43,943	0	2517	0.1	1	ı	_		20
0.5	15	0:030	1.25	3	75,821	41	2508	0.1	ı	I	-	3	21
	10	0.020			74,855	10	2969	0.1	ı	I	<del></del>		22
	7.5	0.015			75,385	8	3111	0.1	ı	I	<del></del>		23
	6.25	0.0125			73,701	7	3392	0.1	0.02	I	-		24
	5	0.010			72,294	5	2567	0.1	ı	I	-		25
	3.75	0.0075			96,530	9	2577	0.1	I	I	_		26
	2.5	0.0050			177,79	4/5	2615	0.1	ı	I	-		27
	1.25	0.0025			16,1379	5	1149	0.1	ı	I	-		28
	0	0.000			68,316	0	2597	0.1	1	ı	-		29

Table 1 (continued)

Panel height	Panel height Channel width	ı	Distance from panel to the ceiling	Room wall height	Mesh cells Cell rows in Channe Width	Cell rows in Channel Width	Total iterations	Total iterations Initial time step subrelax factor	Next time step subrelax factor	Next time step subrelax factor	Class	Class Model Case	Case
٩	s	s/h	h1	¥	ı	ı	ı	ı	ı	ı	ı	ı	ı
٤	mm	Ratio	E	٤	n°	n°	n°	ı	ı	ı	ı	ı	ı
2	40	0.020	3.50	9	86,321	16	2189	0.1	0.02	0.01	2	4	30
	20	0.010			72,953	80	6839	0.1	0.02	0.01	2		31
	10	0.005			12,5094	8	1772	0.1	I	ı	2		32
	2	0.0025			13,9375	9/15	2352	0.1	ı	ı	2		33
	ĸ	0.0015			14,4616	6/9	3101	0.1	0.02	0.01	2		34
	2	0.0010			18,2261	5	2474	0.1	0.02	I	2		35
	0	0.000			77,784	0	4113	0.1	0.02	0.01	2		36
2	* 04	0.02	3.5	9	10,2612	19	2825	0.1	0.02	0.007	4	5	37
_	20	0.020	4	9	94,336	16	2327	0.1	0.02	0.01	2	9	38
	10	0.010			83,360	6	5953	0.1	0.02	ı	2		39
	5	0.005			70,471	4	2141	0.1	ı	ı	2		40
	4.2	0.0021			17,1693	9/11	2888	0.1	0.02	0.01	2		41
	3.5	0.0018			17,5508	6//	2413	0.1	0.02	ı	2		42
	2.5	0.0013			17,3025	9	4470	0.1	0.02	ı	2		43
	0	0.000			73,057	0	4285	0.1	0.02	ı	2		44
Only wall 3 m height model	height model												
0	0	0.000	0.0	3	22,494	ı	1157	0.1	ı	ı	Ω	7	45

Advection scheme: hybrid for all the cases. Maximum residual allowed: 5.0E-06\*In this case (37) there is a  $15 \times 5$  cm cornice, 30 cm above the panel

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all the CFD mesh elements in the room (between 43943 and 182261). Thus, we have exported the temperatures and heat fluxes distribution from 100 points located in three vertical layers along the panel height: along the *Back*, along the *Front* and along the *Wall*. Knowing these temperatures distribution and the SH in the room, we have calculated the RH values in these same 100 points for the two SH scenarios.

Besides, we also got the air velocities and turbulence intensity along the *channel* that helps to improve the understanding of the heat and mass transfer through the *channel*. Comparing the exported values, we have seen that in addition to the classical non-dimensional number *s/h* (*channel* width/wood panel height) there are other parameters (as the distances from the ceiling to the panel or the possibility of eddies at the *channel* inlet and outlet) that can modify the temperature and the heat flux distribution in the *channel*.

## Heat transfer parameters and room conditions Walls and wood panel heat conduction

The room floor, the roof and the inner wall are adiabatic. The exterior wall is limestone 41 cm thick, and includes a 1 cm mortar layer. The exterior wall parameters are: thermal conductivity  $k_h = 1.8$  W/m K, density  $\rho = 2095$  kg/m³, and specific heat or fluid heat capacity cp = 903 J/kg K, all including the correction factor for the mortar layer. The parameters used for the wood panel are:  $k_h = 0.2$  W/m K,  $\rho = 700$  kg/m³, and  $c_p = 1600$  J/kg K.

Although as stated in the Fourier equation  $\rho c_p \frac{\partial T}{\partial t} = 0$ , with T for temperature and t for time, the  $\rho$  and  $c_p$  values are not required for heat fluxes through solid materials in steady conditions (see Additional file 1: Appendix S2.1 point D), we use them in the calculations as they are required for the transient approach, with a virtual time factor, used to get a more stable convergence (see Additional file 1: Appendix S2.2) As in this study we are not concerned with the real time needed to reach the steady condition, the temperature and heat flux obtained are applicable to other exterior walls and hung panels provided with correlated conductivity materials and widths (same width \*  $k_h$ ).

Outdoor air temperature set for all the simulations is -3 °C and outdoor *heat convection boundary film coefficient* has been considered to be 25 W/m<sup>2</sup>K as recommended for building heat load calculations under normal wind conditions.

#### Heating by air convection

In order to maintain temperature in the room at  $19.6~^{\circ}\text{C} \pm 0.3~\text{K}$  (except for the four corners and a narrow area near the exterior wall and the floor) we have simulated a forced convection system blowing air into the

room at 20 °C and at 1 m/s for a room 3 m high. In this 2D simulation, the air enters the room through a grille 0.1 m high, located on the upper corner of the opposite wall from the wood panel. The air direction is shifted by the grille -15 °C from the horizontal axis to counteract part of the Coanda effect. The air is exhausted by an identical grille near the floor level in conservative conditions. Done this way, we achieve a very homogeneous temperature distribution without stratification.

Air supplied in models with rooms 6 m high is blown at 2 m/s and 20 °C (instead of 1 m/s) to compensate heat losses through the exterior wall which is twice the area of the wall 3 m high and to achieve the 19.6 °C  $\pm$  0.3 K in the room.

Inside the room the air conduction heat coefficient used in the boundary layer laminar flow is 0.0255 W/m K.

#### SH scenarios

Two different SH scenarios, both within the range of proper museum conditions, have been set out to calculate the RH values in the different areas of the room, according to the temperatures computed in the CFD models and cases. In this way the *channel* microclimate was correctly quantified. The conditions for both scenarios are the following:

Scenario SH1: 52% RH in a room heated at 19.6 °C with a Dew Point of 9.7 °C and a SH = 7.5 g water/kg air, which corresponds to high occupation (5 m<sup>2</sup>/person) + natural infiltration at 1 Volume/h with outside air at -3 °C and 90% RH.

Scenario SH2: 60% RH in a room heated at 19.6 °C with a Dew Point of 11.9 °C and a SH=8.7 g water/kg air, which corresponds to middle occupation (8 m $^2$ /person)+natural infiltration at 0.5 Volumes/h with outside air at -3 °C and 90% RH.

#### RH criteria for the proper conservation of the artistic assets

To guarantee the proper conservation of the artistic assets, the following two criteria have been set: 1) RH in the panel Back must be < 66%; 2) If RH in the Wall = 100%, at least "s"  $\geq$  2 cm.

The first criterion corresponds to the Smithsonian Institution standard for RH in exhibition rooms released in 2007 [16] which established the range from 37% to 53% and was extended by Erhardt et al. [17] to 30% < RH < 60% after the tests performed on different art materials such as wood, pigments, paint layers, gesso, etc. Also the present ASHRAE conditions [16, 18, 19] can be met with two options for class A (this class foresees small risk of mechanical damage to high vulnerability artifacts and no mechanical risk to most artifacts, paintings, photographs, and books). The first one is RH from 35 to 65% with the set point at 50%, allowing ± 10% seasonal set

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point variations and  $\pm\,5\%$  short term fluctuations. This option allows to extend the RH up to 65%. The second one is RH within the range of 40–60% with 50% as a permanent set point for the whole year and  $\pm\,10\%$  short term fluctuations.

Our second criterion—a minimum separation of 2 cm between the panel *Back* and the *Wall* when this later is at 100% RH—is under review and it is considered only as a temporary solution in the case that it is impossible to change the painting location or to improve the exterior wall isolation, as it usually happens in some historical buildings.

Actually others standards as EN 15757 [20], EN15759-1 [21] and EN 15759-2 [22] are developed to deal with climate at historical buildings, churches and chapels where wood panels and easel paintings have been submitted to important RH variations along the centuries and have been adapted to the climate conditions showing visible effects such as cracks and flakes or not visible as plastic strains. In these cases, changing the historical climate conditions for others theoretically better may lead to a more endangered condition of the weak artwork.

These standards allow the seasonal RH set point to move in a broader range (safe band), according to the computed mean average (CMA) calculated after 13 months of measured RH inside values and the conservators criteria about the exposed or stored artwork condition, as Camuffo [23, 24], Bratasz [25, 26], Broström et al. [27], Neuhaus and Schellen [28], Schijndel [29] and others have explained.

Today the room RH control in exhibitions and museums varies according to the institutions economic saving policy and energetic goals, the condition and history of exposed or stored objects, the wall materials and air tightness, the importance of the visitors comfort, and other factors.

In order to simplify, in our research we have used, as RH threshold, the maximum allowed value in the ASHRAE standard for the A class. It was not possible to give a universal solution to all the real cases, as this involves studying the endless combinations of temperature and RH possible conditions, the different isolation and thermal inertia of the walls, the unlike building shapes, the varying RH buffers, etc. Our goal is to improve the understanding of heat fluxes, RH and temperatures that take place at the back of wood paintings on exhibition hung in peripheral walls in order to provide conservators with the knowledge to be applied in cases with similar conditions.

#### **Complementary cases**

After the analysis of the 45 basic cases, only 3 of them complied the RH values to avoid damages in the artistic

asset. Thus, we have extended the simulations to other complementary cases and by a trial and error procedure we have found the distances required, from the panel to the Wall, to comply with the required RH in each layer. In this way we got 9 complementary cases, all of them in the same conditions as before, but not exceeding the 66% RH in both SH scenarios. In the cases of water condensation in the Wall a minimum of 20 mm from Back to Wall is maintained. Also we have extended the simulations to 2 complementary cases by adding 60 mm of expanded polystyrene (EPS) insulation to the exterior wall and to 2 other complementary cases (channel width 8 mm and 20 mm) adding an aluminium protection layer, 0.5 mm thick, at the Back which improves greatly the Back temperatures. As the 8 mm channel width case has a minimum Wall temperature of 7.3 °C (RH=100%) we cannot recommend it and the 20 mm minimum channel width is recommended for the Wood panel with Aluminium protection. For the isolated wall composition see Table 2.

Like this, we have extended the general recommendation [3] that states a minimum of 20 mm between a painting and an exterior wall, to more detailed specifications according the different situations. In addition we quantified and clarified the heat transfer modes between the *Back* and the *Wall* in these circumstances.

There are other possible variables to take in account, as possible different panel thickness, obstacles to the air flow as cradling, other room or outside temperatures, other inside SH, other geometries, etc., but we have focused in our variables in order to understand and quantify the temperatures, RH and heat fluxes in different conditions, to provide to the conservators the knowledge to understand and deal with the particular conditions they would find.

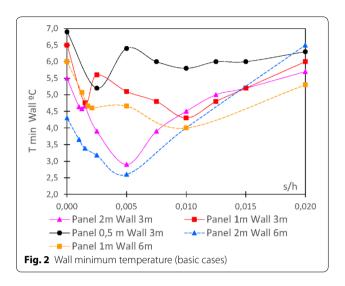
#### Calculation procedure. Equations used

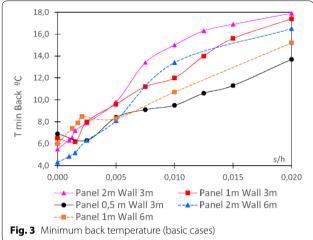
The equations used are the conservation of mass (continuity) equation, the conservation of momentum (Navier-Stockes) equations, the conservation of energy (transport equation for enthalpy) equation and the heat transfer through solids (wall and wood panel) equation which it is the Fourier equation but without internal heat production.

Table 2 Isolated wall parameters for two complementary cases

Material	Layer	Width	Thermal conductivity
		cm	W/m K
Concrete block	Outside	25	1
EPS insulant	Internal	6	0.038
Ceramic brick	Inside	10	0.6

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All these equations are developed in Additional file 1: Appendix S2.1

The procedure used to solve these equations in a steady flow is shown in Additional file 1: Appendix S2.2

The boundary and initial conditions used to solve these equations are shown in Additional file 1: Appendix S2.3

#### Results

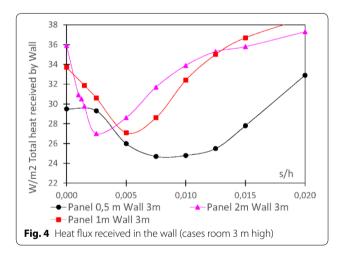
Temperature and heat flux values in 100 points of the CFD simulation, distributed in the vertical axis along the interface layers—*Wall/channel* air, *channel* air/*Back*, and *Front*/room air—have been exported for each case.

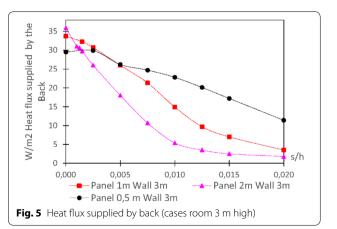
Also for each of the cases, the temperature and the vertical component (v) of the air velocities have been exported from 20 points distributed horizontally along the *channel* inlet between the *Wall* and the panel to compute *Ti*, the *channel* inlet air mean temperature (vertical velocity weighed).

For the cases of the model where the wood panel is 50 cm high, the turbulence intensity (*Tu*) has also been exported in order to compute the turbulence intensity average (*Turb*) at different heights along the *channel*. Doing it in this way, the computed heat fluxes have been assigned to the different convection modes (laminar or turbulent) in the detailed analysis of "Heat fluxes and minimum temperatures in the *Wall* and the Panel *Back*" section.

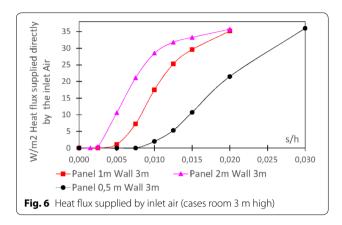
In Figs. 2 and 3 the minimum temperatures in the *Wall* and the *Back* can be seen for all models and cases.

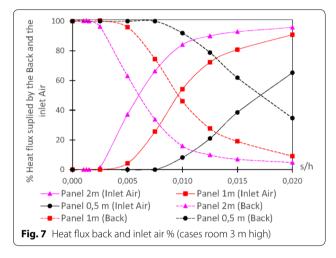
Figures 4, 5 and 6 show the averaged heat fluxes for all models and cases. Figure 4 displays the total heat flux received by the *Wall*, Fig. 5 the heat flux supplied by the *Back* and Fig. 6 the heat flux supplied directly by the air entering the *channel*. Figure 7 shows heat flux ratios





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between *Back* and *Wall* (total) and also between Inlet air and *Wall* (total). In all these graphics heat fluxes and temperatures are plotted versus the "s/h" adimensional number.

Table 3 presents all these values for the 45 main cases together with other parameters such as dimensions, plus the inlet air eddy, if it appears. In addition, RH in the *Wall*, the *Back* and the *Front* are included for the scenarios SH1 and SH2.

For complementary information, see Additional file 1: Table S0.1 in Additional file 1: Appendix S0 with more detailed results for each layer (*Wall, Back* and *Front*).

#### Discussion

## Heat fluxes and minimum temperatures in the Wall and the Panel Back

In Additional file 1: Appendix S1 there is a detailed analysis of the heat fluxes, turbulence and temperatures at different heights in the *channel* between *Back* and *Wall* for all the cases in a 50 cm high panel. It allows to understand the involved phenomena and temperatures distributions in the *channel*.

We can see how the *Wall* temperature decreases as the panel separates from the *Wall*, due to the laminar flow close to the *Wall*, and thus the heat flux is only by conduction. Added to the effects of the eddy locations in the *channel* inlet and *channel* outlet, the temperature attain a minimum at s=1.25 mm. As the *channel* width continues increasing at s=2.5 mm the outlet eddy change its direction and the *Wall* is heated enough to compensate the conduction heat flow reduction and the *Wall* temperature attain a relative maximum.

As the *channel* width continues increasing at s=5 mm, it appears another temperature minimum. If the *channel* width continues increasing and attain s=7.5 mm, the heat flux to the *Wall* increases, as inlet air heat flux increases more than the *Back* heat flux decreases (due to the increasing of inlet air flow and turbulence). This raises the *Wall* temperatures.

From this point the *Back* and *Wall* temperatures increase, approaching the air room temperatures. It is quantified in Additional file 1: Table S1.1 and explained with detail in Additional file 1: Appendix S1.

Figure 2 and Table 3 show how the two *Wall* temperature minimums discussed in Additional file 1: Appendix S1 for a 50 cm high panel also appear for panels with h=1 m (4.8 °C and 4.3 °C) and for panels with h=2 m (4.58 °C and 2.9 °C) in a room 3 m high and for panel with h=1 m (4 °C and 4.6 °C) in a room 6 m high. As h1 (distance from the panel upper border to the ceiling) increases, the difference between the first minimum *Wall* temperature and the intermediate maximum decreases. The intermediate maximum nearly disappears for h=2 m and h1=3 m. As h increases, the second minimum is displaced to lower s/h values (to the left side of the curve in Fig. 2).

The explanation is that as h1 increases, more cooled is the air descending close to the Wall and the Ti (average air inlet channel temperature) is lower. Thus, the air layer cooled by the Wall is wider and more air mass is cooled. This can be seen in the Table 3, column  $T_i$  (Channel inlet air mean temperature, vertical velocity weighed).

However, the phenomenon is not that simple and other factors shall also be considered.

#### The air mass flow going into the channel

It can be seen in the special case for h=2 m, s=40 mm, where the *minimum Wall temperature* for ht=6 m, is higher (6.5 °C) than for ht=3 m (5.7 °C). For ht=6 m, the air mean velocity in the *channel* inlet is 0.6 m/s (at 16.4 °C as average) whereas for ht=3 m it is 0.3 m/s (at 18 °C average). Thus, being the air mass twice for ht=6 m and the air temperature only 1.6 K lower, the inlet air thermal energy level is higher for ht=6 m than for ht=3 m and it provides enough heat to raise the *minimum Wall* 

height	<i>Channel</i> width		Distance from panel to the ceiling	Room wall height	Minir	Minimum temperature	ø	RH at minir temperatur in scenario SH1 (52% R in the room	RH at minimum temperature in scenario SH1 (52% RH in the room)*	<b>E</b> _ *	RH at minir temperatur in scenario SH2 (60% R in the room	RH at minimum temperature in scenario SH2 (60% RH in the room)**		Average heat flux Wall = Back + inlet Air	heat fl ack + ir	ux ilet Air		* * *	Air mean vertical velocity at the <i>channel</i> inlet.	Channel inlet Eddy
I	S	s/h	h1	ht	Wall	Back	Front	Wall	Wall Back Front		Wall	Back Front		Wall B	Back	Inlet Air	Inlet Air/ Wall	Inlet Air/ <i>Channel</i> Wall Inlet	Inlet	Inlet
٤	E	ratio	Ε	٤	ů	ပွ	ů	%	%	%	%	% %		W/m² v	W/m²	W/m²	%	Ç	s/m	N/X
Only wa	Only wall 3 m height model	t model																		
0	0	0.000	0.0	$\sim$	12.6	ı	ı	82.5	1	ı	95.2		9	66.3		66.3	100	ı	I	ı
2	40	0.020	0.5	$\sim$	5.7	17.9	18.1	100	583	57.6	100	67.3 66.	2	37.3	<del>.</del> 8.	35.7	95.8	19.1	0.35	Not
	30	0.015			5.2	16.9	17.3	100	62.2	9.09	100	71.8 70	70.0	35.8	2.5	33.27	92.9	18.9	0.33	Not
	25	0.013			5.0	16.3	16.6	100	64.7	63.4	100	74.7 73	73.2 35	35.3	3.5	31.8	06	18.8	0.33	Not
	20	0.010			4.5	15.0	15.8	100	70.4	8.99	100	81.3 77.1		33.9	5.4	28.5	84.2	18.4	0.32	Not
	15	0.008			3.9	13.4	15.0	100	78.2	70.4	100	90.3 81	81.3 3	31.7	10.7	21.1	66.3	17.8	0.27	Not
	10	0.005			2.9	9.8	11.8	100	9.66	87.0	100	100 100		28.6	<u>∞</u>	10.6	37.1	16.8	0.19	Not
	2	0.003			3.9	7.9	10.1	100	100	97.6	100	100 100	27		26	0.4	4.	9.1	90:0	Not
	3	0.0015			4.65	7.2	9.7	100	100	100	100	.100 100		29.8 2	29.8	0	0	7.1	0.02	Not
	2.5	0.0013			4.58	8 6.5	9.1	100	100	100	100	100 100		30.5 3	30.6	-0.08	0	6.7	0.02	Not
	2	0.0010			4.64	6.3	9.1	100	100	100	100	100 100		30.9	31	-0.08	0	7.0	0.01	Not
	0	0.000			5.5	5.5	8.1	100	100	100	100	100 100		35.9 3	35.9	0	0			
-	20	0.020	1.0	3	0.9	17.4	18.1	100	60.2	97.6	100	99.5 66	66.5 38	38.7	3.5	35.2	6.06	17.3	0.36	Not
	15	0.015			5.2	15.6	16.8	100	67.7	9.79	100	78.2 72	72.3 30	36.7	7	29.6	80.8	16.6	0.30	Not
	12.5	0.013			4.8	14.0	15.5	100	75.2	68.1	100	86.8 78	78.7 35		9.7	25.3	72.3	16.0	0.27.	Not
	10	0.010			4.3	12.0	14.1	100	85.9	74.7	100	99.1 86	86.2 3.	32.4	14.9	17.5	54.2	15.2	0.22	Not
	7.50	0.008			4.8	11.2	13.7	100	9.06	7.97	100	100 88	88.5 28	28.6 2	21.3	7.3	25.6	15.0	0.14	Yes
	2	0.005			5.1	9.6	12.3	100	100	84.2	100	100 97	97.2 2.7	27.1 2	26	1.1	4.3	14.1	0.07	Yes
	2.5	0.003			5.6	8.0	11.3	100	100	0.06	100	100 100		30.6	30.7	0	0	10.5	0.02	Yes
	1.5	0.0015			4.8	6.2	9.5	100	100	100	100	100 10	100 3	31.9 3	32.3	- 0.4	0	7.9	0.01	Yes
	0	0.000			6.5	6.5	9.5	100	100	100	100	100 100		33.7 3	33.7	0	0			
0.5	15	0.030	1.25	3	7.5	.16.3	3 17.2	100	64.7	61.0	100	74.7 70	70.4 4.	41.5	5.4	36	87	16.1	0.34	Not
	10	0.020			6.3	13.7	15.3	100	7.97	0.69	100	88.5 79	79.7 3.	32.9	1.4	21.5	65.3	14.2	0.25	Not
	7.5	0.015			0.9	11.3	13.5	100	0.06	77.7	100	100 89	89.7 2.	27.8	17.2	10.7	38.5	12.9	0.18	Yes
	6.25	0.013			0.9	10.6	12.9	100	94.3	6.08	100	100 93	93.3 2.	25.5 2	20.1	5.3	21	12.5	0.13	Yes
	2	0.010			5.8	9.5	12.0	100	100	85.9	100	100 99.1		24.8 2	22.8	2	8.2	11.4	60:0	Yes
	3.75	0.008			0.9	9.1	11.9	100	100	86.4	100	100 99	99.8	24.7 2	24.7	0.0	0	10.0	0.05	Yes
	2.5	0.005			6.4	8.4	11.2	100	100	9.06	100	100 100	26		26.2	0	0	8.3	0.02	Yes

Table 3 (continued)

Panel height	Channel width		Distance from panel to the ceiling	Room wall height	Minin	Minimum temperature		RH at minimu temperature in scenario SH1 (52% RH in the room)*	RH at minimum temperature in scenario SH1 (52% RH in the room)*		RH at minimur temperature in scenario SH2 (60% RH in the room)**	RH at minimum temperature in scenario SH2 (60% RH in the room)***	Ave Wal	Average heat flux Wall = Back + inle	Average heat flux Wall = Back + inlet Air		***	Air mean vertical velocity at the <i>channel</i> inlet.	Channel inlet Eddy
I	Ŋ	y/s	ħ1	ht	Wall	Back	Front	Wall E	Back Fr	Front V	Wall Bo	Back Front	nt Wall	I Back	Inlet Air	Inlet Air/	' <i>Channel</i> Inlet	Inlet	Inlet
٤	m m	ratio	٤	Ε	ů	ů	ů	%	% %		% %	%	W/m²	n² W/m²	<sup>2</sup> W/m <sup>2</sup>	%	ů	s/m	N/A
	0	0.000			6.9	6.9	9.8	1001	56 001	9.66	100 10	001 001	29.5	29.5	0	0			
2	40	0.020	3.50	9	6.5	16.5	16.8	100	63.9 6.	62.6	300	3.7 72.3	3 37.8	1.7	36.1	95	16.4	0.63	Not
	20	0.010			4.0	13.4	13.9	100	78.2 75	75.7	00 001	90.3 87.4	1 30.8	5.8	25	81	15.2	0.40	Yes
	10	0.005			5.6	8.1	9.6	100	100 10	100	100 10	100 100	24.2	15.9	8.2	34	15.0	0.17	Yes
	2	0.0025			3.2	6.3	8.2	100	100 10	1 00	100 10	100 100	24.9	24.2	0.7	0.03	12.0	0.05	Yes
	$\sim$	0.0015			3.4	5.2	7.1	100	100 10	1 00	100 10	100 100	26.9	26.8	0.05	0.00	9.7	0.00	Yes
	2	0.0010			3.7	4.8	8.9	100	100	100	00 10	100 100	28.1	28.0	0.02	0.01	9.6	0.01	Yes
	0	0.000			4.3	4.3	6.3	100	1000	100	100 10	100 100	33.4	. 33.4	0	0			
-	20	0.020	4.00	9	5.3	15.2	15.9	100	99.5 66	66.4	100 8C	80.2 76.6	5 34.2	5.6	28.7	83	14.6	0.42	Yes
	10	0.010			4.0	10.7	12.6	100	93.7 82	82.5	100 10	100 95.2	2 27.4	. 13.9	13.5	49.	13.7	0.27	Yes
	2	0.005			4.66	8.3	10.8	100	36 001	93.1 1	00 10	100 100	25.2	24.2	1.0	4	10.4	0.07	Yes
	4.2	0.0021			4.60	8.5	11.1	100	100 9	91.2	00 10	100 100	26.1	25.7	0.4	0	11.2	0.05	Yes
	3.5	0.0018			4.66	7.9	10.7	100	9001	93.7 1	00 10	001 001	26.3	26.2	90:0	0	0.6	0.04	Yes
	2.5	0.0013			5.1	7.4	10.3	100	100 96	96.3 1	00 10	001 001	27.8	3 27.7	0.01	0	8.5	0.02	Yes
	0	0.000			0.9	0.9	9.0	100	100 10	100	00 10	001 001	32.2	32.2	0	0	ı	ı	1
2	****	0.020	4.00	9	3.6	13.5	14.1	100	77.7	74.7	100 89	89.7 86.2	2 27.9	3.5	24.4	87.3	16.8	0.16	Yes

\*\$H1 = 7.5 g water/kg air; dew point = 9.7 °C; room at 19.6 °C and 52% RH; outside at - 3 °C \*\*\$H2 = 8.7 g water/kg air; dew point = 11.9 °C; room at 19.6 °C and 60% RH; outside at - 3 °C

Bolditalic: minimum  $\mathit{Wal}$  temperature; italic: condensation; bold: RH < 66%

<sup>\*\*\*</sup>T = Channel inlet air mean temperature, vertical velocity weighed \*\*\*\*In this case (37) there is a 15  $\times$  5 cm cornice, 30 cm above the panel

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temperature up to 6.5 °C. When "s" diminishes, as in the case of h=2 m and s=20 mm, the minimum Wall temperature is 4 °C for ht=6 m (inlet velocity 0.4 m/s at 15.2 °C) and 4.5 °C for ht=3 m (inlet velocity 0.32 m/s at 18.4 °C). In this case, the air velocities are closer and the inlet air thermal energy level is lower for ht=6 m than for ht=3 m. An intermediate case is for h=2 m, s=30 mm where the minimum Wall temperatures are the same for ht=6 m and for ht=3 m (5.2 °C).

#### The air turbulence in the channel

For small values of "s" (channel width), the air flux is laminar and the heat transfer from the Back is only by conduction. This heat flux diminishes lineally as "s" increases, but as "s" increases more inlet air goes into the channel and the inlet air becomes the heat flux mean supplier to the Wall. As the channel air flow increases the heat flux turns to be turbulent and the addition of the both effects results in the curve "s/h" versus heat flux with a minimum in the zone where the inlet air heat flux starts (s/h between 0.003 and 0.01). This phenomenon can be observed in the three curves of Fig. 4 which are, in turn, composed by the curves of Figs. 5 and 6. The minimum in these curves moves to the right side of the chart as the panel height decreases. In order to further clarify this, Fig. 7 gathers these curves expressed as a percentage.

Also, as shown in Additional file 1: Appendix S1, when the *channel* is very narrow, air turbulence decreases as the air goes down inside the *channel*. In these cases, the air flux becomes laminar, still if it has been turbulent just near the *channel* inlet.

Depending on Temperatures, "s" and "h" parameters, the minimum temperature occurs at mid-height or at the lower zone of the *channel*. (See Additional file 1: Appendix S0, Table S0.1).

#### The eddy in the channel inlet

The widening of the air layer descending close to the *Wall* due to large values of *h1* and the narrowing of the *channel* can form an air eddy in the *channel* inlet, as more mass of the cooled air descending close to the *Wall* collides with the top edge of the panel. In this way the air going down close to the *Wall* gets mixed with the air of the room that enters the *channel*. This smooths the temperature differences in the *channel* inlet between the *Back* and the *Wall*. The developed eddy is shown in Figs. 8, 9 and 10.

Table 3 shows in which cases an eddy is developed at the inlet.

#### The eddy in the channel outlet

Usually one or more air eddies appear in the channel outlet. Depending on the position of these eddies, heated air of the room around the outlet can get mixed with the cooled air of the channel. This may cause heating of the Wall just under the channel. For example, in the case of a panel 50 cm high and a channel width of 2.5 mm (case 27), the Wall under the panel is heated enough by the outlet eddy to send heat flux by conduction through the Wall in vertical direction, raising the minimum temperature in the Wall (see Fig. 11 for s=2.5 mm). In this same case, this factor explains the maximum of 6.4 °C in the "Wall minimum temperature" compared to the two neighbouring minimums of 5.2 °C that occur when s = 1.25 mm where the eddy is too weak to heat the *Wall* enough and 5.8 °C when s = 5 mm where the heated air of the room is not sent to the Wall near the channel outlet and, instead, the cooled channel air flows into the room (see Table 3 and Fig. 11 with s=5 mm).

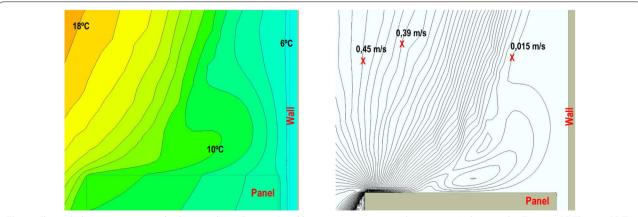


Fig. 8 Channel inlet temperature and velocity isolines. Case 28. Panel h = 50 cm. s = 1.25 mm. h1 = 1.25 m. Values at inlet: Tw = 5.7 °C, Tb = 6.7 °C. Taverage = 6.4 °C. Air channel vertical mean velocity = 0.01 m/s.  $\Delta$  v between isolines = 0.015 m/s. Inlet eddy

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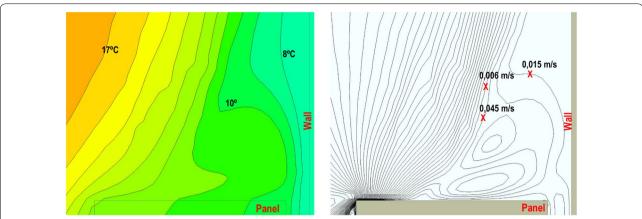


Fig. 9 Channel inlet temperature and velocity isolines. Case 27. Panel h = 50 cm. s = 2.5 mm. h1 = 1.25 m. Values at inlet: Tw = 6.8 °C, Tb = 8.6 °C. T average = 8.3 °C. Air channel vertical mean velocity = 0.02 m/s.  $\Delta$  v between isolines = 0.015 m/s. Inlet eddy

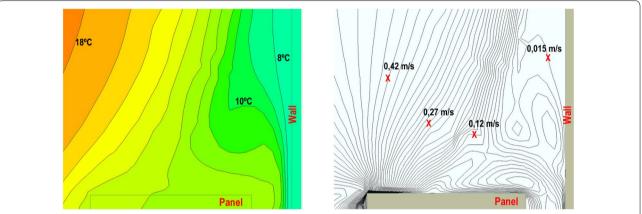


Fig. 10 Channel inlet temperature and velocity isolines. Case 25. Panel h = 50 cm. s = 5 mm. h1 = 1.25 m. Values at inlet: Tw = 7.8 °C, Tb = 11.2 °C. T average = 11.4 °C. Air channel vertical mean velocity = 0.09 m/s.  $\triangle$  v between isolines = 0.015 m/s. Inlet eddy

#### Cornices over the panel

In the case of a cornice protruding from the *Wall* (s=40 mm, case 37) it can be seen that the minimum temperatures in each layer are at least 3 °C lower that in the case with a straight *Wall*, due to the air flux deviation at the cornice and the eddy developed below it, that reduces the entrance of hot air from the room to the *channel*. So, the mean air temperature, vertical velocity weighed at the *channel* inlet, is reduced from 0.62 to 0.16 m/s (compared to the same geometry without cornice as it is the case 1) and still if the mean air temperature at this point is increased from 16.4 to 16.8 °C, the mean heat flux received by the *Wall* in the *channel* drops from 36.1 to 27.9 W/m² (see Table 3).

In order to compensate the *Back* and *Wall* temperature reduction and the heat flux reduction which occurs in this case, and to get the correct temperatures and RH values in the *Back*, it is necessary to increase the *channel* 

width from 40 to 90 mm in scenario SH1 and from 85 to 140 mm in scenario SH2 (see Tables 4 and 5).

#### RH values in the different cases

Table 3 also shows the maximum RH values of the significant layers (*Wall*, *Back* and *Front*) for scenarios SH1 and SH2. In both scenarios condensation appears on the *Wall* and, in many cases, RH values in the *Back* are above 66%, which is the limit set for the proper conservation of paintings.

## Minimum required distances from a painted wood panel to the exterior wall

From the results of the 3 basic cases, that comply with the two conservation criteria set in Sect. 2.3, and the 13 complementary cases, we got a set of 8 cases for the SH1 scenario (room RH of 52% at 19.6 °C) and other set of 8 cases for the SH2 scenario (room RH of 60% at

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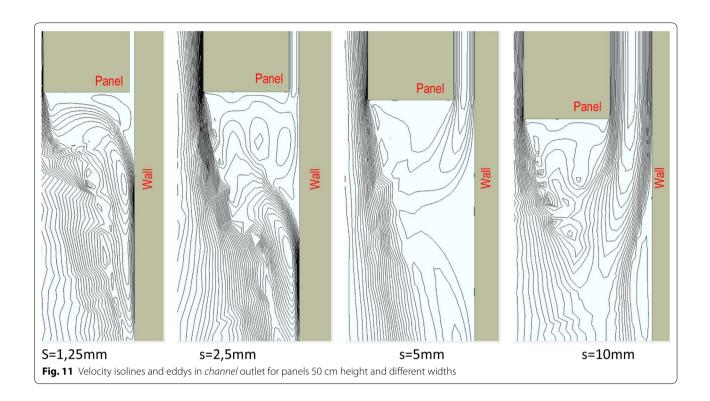


Table 4 Minimum "s" distances in scenario SH1

Panel height	Minimum Channel widt	h	Distance from panel to ceiling	Room wall height	Minimu	um tempei	ature		ninimum T ario SH1 (5 oom)	•
	s	s/h	h1	ht	Wall	Back	Front	Wall	Back	Front
m	mm	ratio	m	m	°C	°C	°C	%	%	%
2	25	0.013	0.5	3	5.0	16.3	16.6	100	64.3	63.1
1	20	0.020	1.0	3	6.0	17.4	18.1	100	59.9	57.2
0.5	20	0.040	1.25	3	7.6	17.5	18.1	100	59.5	57.2
2	40	0.020	3.50	6	6.5	16.5	16.8	100	63.5	62.2
1	30	0.030	4.00	6	6.5	16.8	17.3	100	62.3	60.3
2	90*	0.045	3.50	6	5.1	16.2	16.3	100	64.7	64.3
Isolated wall 2 m	height with 60 m	ım EPS								
2	20	0.010	0.50	3	13.7	17.2	18	76.2	60.7	57.6
Back protected v	vith Aluminium la	yer 0.5 mm w	idth							
2	20	0.010	0.5	3	5.3	19.4	18.9	100	52.0	54.4

 $If there is condensation in the wall (100\% RH), the minimum required gap between the Wall and the painting to avoid damages is 20 \ mm$ 

Room width 3 m. Outside wall: limestone (1.8 W/m\*K), width 40 cm

SH = 7.5 g water/kg air; Dew Point = 9.7 °C; Room at 19.6 °C and 52% RH; Outside at - 3 °C

\*In this case there is a  $15 \times 5$  cm cornice, 30 cm above the panel

 $19.6~^{\circ}\text{C})$  which comply with these conservation criteria. From these 16 cases we got the correct *channel* widths for all the models analysed.

Table 4 presents the 8 recommended minimum *chan-nel* widths for the scenario SH1 and Table 5 the same figures for SH2.

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Table 5 Minimum "s" distances in scenario SH2

	Minimum <i>Channel</i> width	1	Distance from panel to ceiling	Room wall height	Minimu	ım tempera	ture		ninimum tei ario SH2 (60 n)	•
h	S	s/h	h1	ht	Wall	Back	Front	Wall	Back	Front
m	mm	ratio	m	m	°C	°C	°C	%	%	%
2	50	0.025	0.5	3	5.8	18.4	18.5	100	65.2	64.8
1	35	0.035	1.0	3	6.8	18.8	19.0	100	63.6	62.8
0.5	30	0.060	1.25	3	7.9	18.7	18.9	100	64.0	63.2
2	85	0.043	3.5	6	7.0	18.6	18.6	100	64.4	64.4
1	65	0.065	4.00	6	7.4	18.5	18.6	100	64.8	64.4
2	140*	0.07	3.50	6	6.0	18.3	18.4	100	65.6	65.2
Isolate	d wall 2 m height w	rith 60 mm EP:	5							
2	30	0.015	0.50	3	14.2	18.5	18.6	85.7	64.8	64.4
Back p	rotected with Alum	inium layer 0.5	mm width							
2	20	0.010	0.5	3	5.3	19.4	18.9	100	61.2	63.2

If there is condensation in the wall (100% RH), the minimum required gap between the wall and the painting to avoid damages is 20 mm

Room width 3 m. Outside wall: limestone (1.8 W/m \* K), width 40 cm

 $SH = 8.7 \text{ g water/kg air; dew point} = 11.9 ^{\circ}\text{C; room at } 19.6 ^{\circ}\text{C} \text{ and } 60\% \text{ RH; outside at } -3 ^{\circ}\text{C}$ 

It shall be taken in account that changes of the *Wall* geometry, as cornices protruding above the painted wood panel, or other obstacles to the air flux can modify the recommended minimum separation distances, increasing them

Attention: If the outside air temperature increases over -3 °C and the 90% RH is maintained, the SH of the infiltration and ventilations will rise. Therefore the inside room SH and RH will be increased and in this case the recommended *channel* width shall be increased according the foreseen *channel* temperatures and the new inside room SH value.

#### **Conclusions**

By means of a 2 dimensional CFD simulation of a heated room (19.6 °C) with a painted wood panel hung in the inside face of a non-isolated exterior wall (-3 °C in the outside face), we have obtained the temperatures, air velocities, and heat fluxes distribution in the *channel* between the wood panel and the exterior wall, for different wood panel heights, different *channel* widths, and different distances to the ceiling.

Based on the temperature data results in the wood panel *Back* and in the *Wall*, RH values have been obtained at the same locations and for two different SH scenarios (7.5 g water/kg air and 8.7 g water/kg air) corresponding to a room at 52% RH and 60% RH respectively, which are within the normal range of conditions for a museum. From these values, we have established, for the foreseen SH scenarios, the minimum distances between

the panel *Back* and the *Wall* required to avoid damages in the painted wood panel (RH < 66% in the panel *Back*) and a minimum of 20 mm in the case there is condensation in the *Wall*.

In addition, factors that affect temperatures distribution and heat fluxes in the *channel* have been analysed for series of discrete values in the normal range of use. In the case of a wood panel 50 cm high, these have been discussed in further detail in order to help understand the heat transfer modes involved in the situation.

The study of these factors that modify temperature distribution in both sides of the *channel*, such as the distance to the ceiling, the *channel* width, the possible eddy near the *channel* inlet or outlet, can be used as guidelines to be applied to other similar situations like other model dimensions or possible obstacles to the air flux in the *Wall* over the wood panel. As examples of this, the effects of a cornice in the *Wall* or the effects of an aluminium protection layer in the *Back* of the panel or an EPS 60 mm isolation in the *Wall* have been quantified to compare with cases without these peculiarities.

This simulation carried out with a commercial 2 dimensional CFD allows to extend the standard 20 mm recommendations for the distances between cold exterior walls and wood panel paintings to a more detailed recommendations for paintings hung on the walls in similar conditions. These recommendations do not entail neither financial costs nor climate variations in the museums and exhibition rooms and conservators can easily apply them.

<sup>\*</sup>In this case there is a 15  $\times$  5 cm cornice, 30 cm above the panel

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For the studied cases, Table 3, *Back* and *Wall* minimum temperatures and maximum RH values, and Additional file 1: Table S0, *Back* and *Wall* minimum temperatures at different heights, show how different these values are from those in the room or near other walls without panels hung on them. When conservators advise how to protect artistic wood panels hung in a poorly insulated peripheral wall, this fact shall be taken into account in addition to the recommendations in the EN standards [20–22].

#### **Supplementary information**

**Supplementary information** accompanies this paper at https://doi. org/10.1186/s40494-020-00376-1.

Additional file 1. Appendices.

#### Abbreviations

Wall: Inner face of the exterior wall; Back: Wood panel surface facing the Wall; Front: Wood panel surface facing the room; channel: Space between Back and Wall; s: Distance between wall and wood panel, channel width (m); h: Wood panel height (m); s/h: Ratio channel width/wood panel height; ht: Room height (m); h1: Distance from ceiling to wood panel upper border (m); V: Velocity vector (m/s); **q**: Gravity acceleration vector (m/s<sup>2</sup>); **I**: Buoyancy force  $\text{vector} = - \ \mathbf{g} \ (\rho - \rho_0) = \rho_0 \ \mathbf{g} \ \beta \ (T - T_0) \ \text{if} \ \rho \ \Delta \ T \ll 1 \ \text{(N)}; \ u\text{:} \ \text{Velocity horizontal}$ component (m/s); v: Velocity vertical component (m/s); x: Horizontal coordinate m. Origin x = 0 at inner wall (left side). (In Fig. 1); y: Vertical coordinate m. Origin y = 0 at floor level. (In Fig. 1); t: Time (s); P: Pressure (Pa); P': Pressure correction (Pa); T: Temperature (K);  $T_0$ : Reference temperature (K); Tw: Inner face temperature of the exterior wall (°C); Tb: Panel back Temperature (°C); Ti: Air channel inlet average temperature, vertical velocity weighed (°C); Tu: Turbulence intensity (%) = 100 RMS ( $\mathbf{v'/v}$ ), being  $\mathbf{v'}$  fluctuations around the average velocity v; Turb: Turbulence intensity average at y height, velocity weighed in 20 channel points at the same height (%); H: Enthalpy (J); k: Kinetic energy ( $m^2/s^2$ );  $k_h$ : Thermal conductivity (W/m K);  $c_n$ : Specific heat or Fluid heat capacity (J/kg K);  $\delta_{ii}$ : Delta Kronecker (i = j,  $\delta_{ii} = 1i \neq j$ ,  $\delta_{ii} = 0$ ); Pr. Prandtl number  $Pr = \mu c_{p,l} k_h$ ;  $\varphi$ : Generic property (velocity, temperature, and others);  $\rho$ : Density (kg/m<sup>3</sup>);  $\rho_0$ : Reference density at  $T_0$  (kg/m<sup>3</sup>); v. Kinematic viscosity  $(m^2/s) = \mu/\rho$ ; vt: Computed turbulent kinematic viscosity  $(m^2/s)$ ;  $\mu$ : Dynamic viscosity N s/m<sup>2</sup> = kg/(m s);  $\mu_i$ : Turbulent viscosity N s/m<sup>2</sup> = kg/(m s);  $\lambda$ : 2° coefficient of viscosity (Lamé); *E*: Turbulent kinetic energy dissipation rate (m<sup>2</sup>/ s<sup>3</sup>);  $\omega$ : Turbulent kinetic energy frequency dissipation (s<sup>-1</sup>);  $\beta$ : Thermal expansion coefficient for perfect gases = 1/Tunits 1/K;  $\Gamma = \mu + \mu_l$ : units N s/  $m^2 = kg/(m s); \Gamma_h$ : Heat diffusion coefficient  $= \Gamma_h = \left(\frac{\mu}{P_f} + \frac{\mu_t}{P_{f_t}}\right) c_p; \Phi$ : Magnitude to be computed in each cell; RH: Relative humidity (%); SH: Specific or absolute humidity (kg water/kg air);  $\alpha_1$ ,  $\alpha_2$ ,  $\beta_1$ ,  $\beta_2$ ,  $\sigma_{k1}$ ,  $\sigma_{k2}$ ,  $\sigma_{\omega 1}$ ,  $\sigma_{\omega 2}$ ,  $\sigma_{\beta}$ ,  $a_1$ : Turbulence closure constants; Rr: Normalized Euclidian residual (general); Rm: Normalized Euclidian residual for mass.

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#### Authors' contributions

The order of authors in this paper has been set applying the *sequence-determines-credit* approach (SDC). SF analyzed and interpreted the data resulting from software and carried out the calculation procedure and was a major contributor in writing the manuscript. GC-F designed the models and scenarios, provided conservation literature background and contributed in the discussion of results. CR-R collaborated in the analysis of data performing the graphics, images and tables and prepared the manuscript for final publication. MOF participated in the discussion of the results from the conservation point of view and contributed significantly in the writing process. All authors read and approved the final manuscript.

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#### Availability of data and materials

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#### **Competing interests**

The authors declare that they have no competing interests.

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